

RESEARCH ARTICLE

Establishment of a scalable manufacturing platform for *in-silico*-derived ancestral adeno-associated virus vectors

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Adeno-associated virus (AAV) is an effective viral vector for gene therapy due to its non-pathogenicity, high transduction efficiency, broad tissue specificity and long-term transgene expression activity. As such, AAV has become a vector of choice with over 120 active clinical trials worldwide. With this increased demand also comes the need for scalable GMP manufacturing processes that are robust and can support large-scale production. However, current manufacturing of AAV vectors for gene therapy is labor-intensive, resulting in high production costs (adherent-based process) or taking much longer to establish (e.g. producer cell line). Here we report the establishment of a scalable manufacturing platform for AAV production based on transient triple transfection of suspension HEK293 cells. Through flow cytometry, limiting dilution and productivity screening, we first isolated a high producer clonal suspension HEK293 cell line. After medium selection and transfection optimization, we scaled up the production process to 50-Liter using single use bioreactors (SUB). The platform was initially developed for a novel AAV vector (Anc80), that belongs to a large family of novel AncAAV's, as described previously by Luk Vandenberghe [1] but has also been used for the successful production of other AAV serotypes. Using affinity chromatography followed by ion exchange chromatography, we successfully purified the recombinant AAV/Anc80 products with a high percentage of full viral particles. Taken

together, we have established an effective, cost-efficient and scalable manufacturing process for AAV/Anc80 that supports the ever-growing production demands in the AAV gene therapy market.

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INTRODUCTION

AAV has emerged as a key gene therapy vector due to its unique characteristics, including a high safety profile and long-term gene expression activity in humans [2]. There are more than 120 clinical trials using AAV vectors worldwide and the first AAV-based gene therapy in the United States for inherited retinal disease was approved in December of 2017. The fast-growing demand for recombinant AAV in gene therapy highlights the requirement for emerging technologies to develop scalable and improved AAV manufacturing platforms [3].

AAV is a ~25-nm, non-enveloped and non-autonomous virus from the family of *Parvoviridae* [2]. The AAV genome is composed of 4.7 kb linear single-stranded DNA that comprises genes encoding for replication (Rep), capsid (Cap), and virus assembly (AAP) proteins, flanked by inverted terminal repeats (ITR) on both ends. However, these genes are not sufficient for AAV replication in host cells. The reproduction of AAV is dependent on the co-infection of helper viruses, such as Adenovirus, Herpes Simplex Virus, etc. Specifically, five Adenovirus genes were identified that were necessary and sufficient for AAV production in permissive cells, i.e. E1A, E1B, E2A, E4Orf6, and VA. For example, functional recombinant AAV (rAAV) can be readily replicated and assembled in HEK293 cells (expressing

endogenous E1A and E1B) via triple transfection of pHelper vectors expressing additional helper genes (E2A, E4Orf6 and VA), pRep/Cap vector encoding for Rep and Cap proteins, and AAV transfer vector with ITR-flanked transgene or gene of interest (GOI) (Figure 1) [4–6]. Recently, several groups reported the development of fixed-bed or single-use bioreactor based processes for large-scale AAV production via transient transfection. However, these processes were either based on adherent HEK293 cells or dependent on ultracentrifugation for the downstream processes [7–9]. Therefore, an efficient and fully scalable system (both upstream and downstream) for AAV production by transient transfection remained to be developed.

Several different naturally occurring serotypes of AAV are used in gene therapy, e.g., AAV1 for lipoprotein lipase deficiency, AAV2 for inherited retinal disease, and AAV8 and others for hemophilia [10–12]. These serotypes were chosen based on the target tissues. Additional and new serotypes were identified through search of human and nonhuman primate tissues, rational design, and directed evolution [13–15]. However, up to 70% of people have had prior exposure to some AAV serotypes and have thus developed pre-existing immunity (PEI) [16]. PEI renders the AAV treatment ineffective and excludes the majority of patients from clinical trials and therapies. In an effort

to construct new AAV serotypes to reduce the impact of PEI, as well as to identify novel serotype that can target a variety of tissue types, Vandenberghe's lab applied the ancestral sequence reconstruction (ASR) analysis to predict the putative novel AAV capsid sequences, which led to the isolation of a functional and potent AAV lineage, Anc80L65 [1]. The lineage has been the most extensively studied member of this Anc AAV library (~37,000 novel capsids) [17,18].

Here we show that we have established a productive and scalable manufacturing platform for Anc80 vectors using transient transfection in suspension HEK293 cells. We specifically isolated one 'super-clone' with productivities in the range of $2\sim 3E+04$ vg/cell for Anc80, comparable to or better than other available HEK293 suspension cell lines. An upstream process optimized for media and cell densities was successfully scaled

up to 50L in single use bioreactors. Downstream processes using both capture and polishing columns resulted in highly pure full viral particles with potent infectivity in culture. Therefore, the high-production HEK293 manufacturing platform is an excellent option for the clinical and commercial production of Anc80 and other serotypes of AAV vectors.

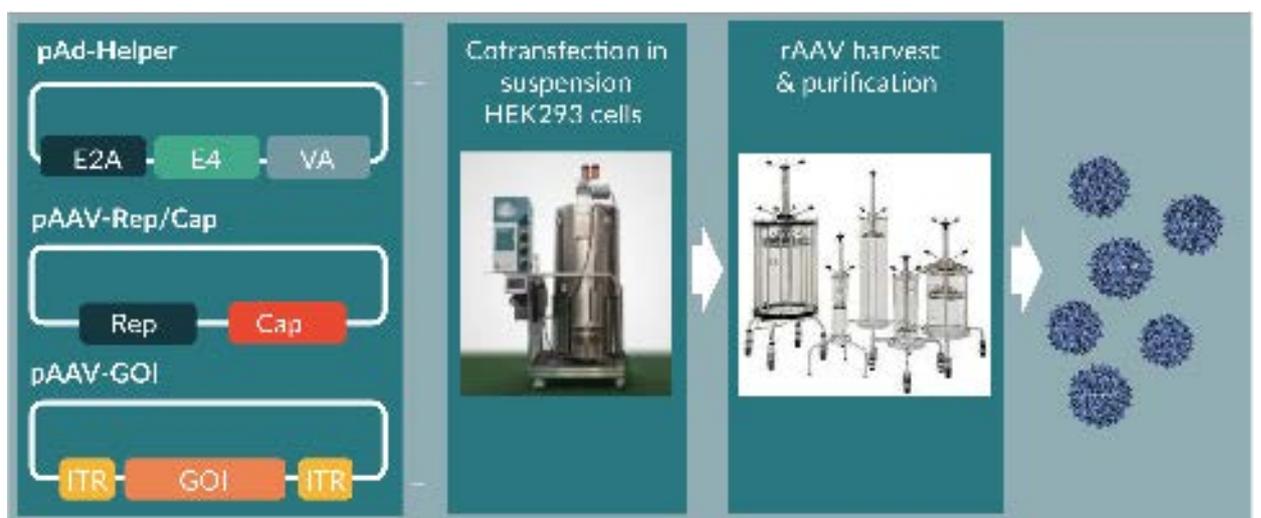
MATERIALS & METHODS

Single cell cloning

HEK293.3sus (Human Embryonic Kidney Cells) were obtained from ATCC (ATCC® CRL-1573.3™, Manassas, VA, USA). Commercially available HEK293 suspension cells (Life Technologies, Grand Island, NY, USA) were used as a control. HEK293.3sus cells were sorted using fluorescence-activated cell sorting (FACS, BD FACSAria II,

► FIGURE 1

AAV manufacturing via triple transfection in suspension HEK293 cells.



Three plasmids for Ad5 helpers (pAd-Helper), AAV Rep and Cap (pAAV-Rep/Cap) and AAV transfer vector for gene of interest (pAAV-GOI) are co-transfected into suspension HEK293 cells in single-use bioreactors. Three days later, recombinant AAVs are harvested and subjected to downstream column purification for purified viruses.

San Jose, CA, USA) into two populations (GFP-high and -medium) based on the level of transfection efficiency using a plasmid encoding for GFP. The cell population displaying medium level transfection efficiency was chosen for limiting dilution into single cell in each well with 1% Penicillin-Streptomycin (Life Technologies, Grand Island, NY, USA) and 1% Human Serum Albumin (Octapharma, Lachen, Switzerland) in FreeStyle F17 medium (Life Technologies, Grand Island, NY, USA). Following plating, each well was screened for the presence of single cells under an optical microscope (Olympus, Tokyo, Japan) at 10x magnification. Single cells were monitored for cell growth on a daily basis. As colonies developed and cells in the wells started becoming confluent, the clones were transferred into larger low-adherence vessels until there were enough cells to be transferred into a shaker flask. 0.1% Pluronic-F68 (Life Technologies, Grand Island, NY, USA) was added to reduce shearing stress while shaking at 80 to 120 rpm in 37°C incubator with 8% CO₂.

Medium screening

In an effort to improve productivity, cell growth and productivity were assessed in several commercially available cell culture media. Cells were transferred into each medium to be screened and passaged to 5E5 viable cells / ml for at least 3 times prior to testing productivity. After three passages, cells were transfected in respective cell culture media and AAV titers were determined by qPCR.

Triple transfection

Cells were seeded 1 day (shake flask) or 2–3 days (3 l and 50 l SUB) before transfection, to target achieving a cell density from 1E+06 to 3E+06 vc/ml at transfection. The plasmids used for the transfection were pHelper (Takara Bio, Mountain View, CA), pAAV-GFP (Cell Biolabs, San Diego, CA) and pRep/Cap for Anc80 (Vandenberghe's lab, Boston, MA) or AAV8 (Synthesized by GenScript, Piscataway, NJ, USA). Briefly, the plasmids, PEIpro (Polyplus, Illkirch-Graffenstaden, France) or PEI MAX (Polysciences, Warrington, PA, USA) were diluted separately in Opti-MEM medium (Life Technologies, Grand Island, NY, USA) and then combined. After 15 minutes incubation of PEI and plasmids mix, the complex containing solution was added to the cell culture for transfection. The culture was continued for three days before harvest.

AAV production in 50 l SUB

A frozen vial of suspension HEK293 RCB cells was thawed and cultured in an appropriately sized Erlenmeyer flask (Corning, NY, USA) using FreeStyle F17 medium (Life Technologies, Grand Island, NY, USA) on a shaker in a humidified incubator at 37°C and 8% CO₂. The culture was subsequently passaged into appropriate size of shake flasks every 3 to 5 days until desired amount of cells were achieved to inoculate a 10 l N-1 culture using FreeStyle F17 medium in a 20 l WAVE bioreactor (GE Healthcare Life Sciences, WA, USA). Once the N-1 culture reached a desired cell density, it was used to inoculate a

50 l production culture at a target seeding density of 5×10^5 vc/ml in a 50 l SUB (Thermo Fisher Scientific, Waltham, MA, USA). The culture was sampled daily for cell count and nutrient analysis using Vi-CELL (Beckman Coulter, Indianapolis, IN, USA) and BioProfile FLEX (Nova, Waltham, MA, USA). Once reaching the desired cell density, the culture was transfected via triple transfection using PEI MAX and plasmids complex solution prepared in a WAVE bioreactor. Harvest was initiated 3 days post transfection.

Prior to the commencement of harvest, the culture was sampled for Anc80 AAV titer analysis. The culture was lysed using triton solution (Sigma-Aldrich, St. Louis, MO, USA) and treated with benzonase and magnesium chloride, and mixed with 500 mM sodium chloride prior to clarification. The culture lysate was then clarified using a depth filter and a 0.22 μ m sterile filter (MilliporeSigma, Burlington, MA, USA). The clarified harvest was concentrated ~10 times and diafiltered for 5 di-filtration volumes (DV) by tangential flow filtration (TFF) (Repligen, Waltham, MA, USA). The resulting column load was stored at -80°C before purification.

Affinity AVB-Sepharose-HP Column Purification of 50 l harvest

The purification runs were performed utilizing the AKTA Avant-150 chromatography purification system and UNICORN software. The column load generated and stored at -80°C was thawed in the 37°C water bath and filtered using the 0.22 μ m Sartoguard PES filter. The filtered sample was

loaded onto the VL22 column packed with AVB-Sepharose-HP (GE, Boston, MA, USA) resin at a linear flow rate of 150 cm/hr. The column was equilibrated with AVB Buffer A (50 mM Tris-base, 500 mM NaCl, 0.001% Pluronic-F68, pH8.0) prior to sample loading and washed with the same buffer after sample loading. The vectors were eluted using step elution with 100% AVB Buffer B (50 mM Sodium Citrate, 200 mM NaCl, 0.001% Pluronic-F68, pH3.5). Approximately 3CV of product eluate was collected into a clean bottle containing Neutralizing Buffer (220 mM HEPES, 440 mM Bis-Tris-Propane, 200 mM NaCl, 0.001% Pluronic-F68, pH9.0) to a neutralized product eluate.

Anion-exchange CIMmultus-QA Column Purification of 50 l harvest

The product eluate collected from the AVB-Sepharose-HP column was divided into two equal portions and each portion was purified using an 8 ml CIM-QA column (BIA Separations, Ajdovščina, Slovenia). The AVB column eluate was diluted with Dilution Buffer (20 mM Tris-base, 2 mM MgCl_2 , 0.001% Pluronic-F68, pH 8.0) to lower the sample's conductivity to enable column binding. Prior to sample loading, the column was equilibrated with CIM-QA Buffer A (20 mM Bis-Tris-Propane, 20 mM NaCl, 0.001% Pluronic-F68, pH 9.0). The diluted sample was loaded onto the CIM-QA column at a flow rate of 1.5 CV/min and the column was then washed with CIM-QA Wash Buffer (20 mM Bis-Tris-Propane, 50 mM NaCl,

0.001% Pluronic-F68, pH 9.0). The vectors were eluted using step elution with 100% CIM-QA Buffer B (20 mM Bis-Tris-Propane, 200 mM NaCl, 0.001% Pluronic-F68, pH9.0). The product eluate was collected into a clean bottle. The purified eluates from the two CIM-QA runs were pooled and formulated into an appropriate buffer (PBS, 0.001% Pluronic-F68, pH 7.4) using the 100 kD, 115 cm², MidiKros mPES Hollow Fiber TFF system (Repligen, Waltham, MA, USA). The formulated drug product was sterile filtered and stored at -80 °C.

AAV qPCR titering

The cleared crude or purified samples were diluted 1:100 and further processed by DNase I (Promega, Madison, WI, USA) digestion at 37°C for 1 hour, followed by Proteinase K (Promega, Madison, WI, USA) at 37 °C for 1 hour and at 95°C for 10 minutes. The treated samples were diluted 1:50 and the qPCR was set up with CMV-specific primers and probe. qPCR reactions were processed by LightCycler 480 II qPCR machine (Roche, Basel, Switzerland) using a thermal program as follows: 95°C for 5 minutes, 95°C for 15 seconds, 60°C for 1 minute; and repeated for 40 cycles. AAV titers were determined by comparison with a standard curve generated from linearized pAAV-GOI plasmids.

Flow cytometry analysis

One ml cell culture samples were collected into 1.7 ml Eppendorf tube, including negative control

cells without transfection. After 5-minute centrifugation at 2000 rpm, cell pellets were gently re-suspended in 1 ml PBS. The percentages of GFP-positive cells were measured with BD Accuri C6 Plus (San Jose, CA, USA) following the standard operating procedures.

Silver staining and Western blot analysis

AAV samples were prepared for electrophoresis under reducing conditions by adding 10µl of LDS 4X sample loading buffer (Life Technologies, Grand Island, NY, USA) to 4µl of 10X sample reducing buffer (Life Technologies) and 24 µl of AAV. The samples were then denatured by heating for 10 minutes at 95°C. Duplicate 4-12% BIS-TRIS SDS-PAGE gels (Life Technologies) were loaded at 1E10 vg/lane based on the viral titer as determined by qPCR assay. The gels were electrophoresed in 1xMES running buffer (prepared from 20x stock solution, Life Technologies) at 200V constant for 24 minutes. After electrophoresis one gel was analyzed by silver staining using Silver Quest Staining kit (Life Technologies) following the manufacturer's recommended standard staining protocol. The gel was stained for approximately 8 minutes then the reaction was stopped and the gel was photographed. The second gel was blot transferred to a 0.45 µm PVDF blot using iBlot 2 dry blot transfer system in conjunction with an iBlot2 PVDF Mini Stack (Life Technologies). The resulting PVDF blot was probed with Western Breeze Chromogenic kit for mouse primary antibodies (Life Technologies) following

the manufacturer's protocol. The primary antibody used was an anti-AAV mouse monoclonal antibody to AAV viral capsid proteins VP1, VP2, and VP3 (American Research Products, Waltham, MA, USA) at a 1:1000 dilution. The chromogen was allowed to react on the blot for approximately 7 minutes after which the reaction was stopped and the resulting blot was dried then photographed.

Negative staining for transmission electron microscopy

The purified and formulated samples were sent to Texas A&M University (College Station, TX) Core Laboratory for negative staining and TEM analysis. Briefly, after thawing, samples were vortexed at level 4 for 3 seconds. 1.5 μ l sample was added directly to carbon film and incubate for about 5 minutes without drying. The excess fluid was blotted with filter paper. The sample was rinsed three times on water droplets and blotted with filter paper and stained with 2% PTA or 0.2% UA with the grid tilted at 45 degrees. After blotting off excess stain, the sample was air dried and subjected to TEM analysis.

TCID50 assay

HeRC32 cells were plated at $4E+04$ vc in 50 μ l per well in 96-well plate and incubated at 37 °C in 5% CO₂ incubator for 20 \pm 4 hours. At the day of infection, 3.2 E+08 vp/ml human Adenovirus 5 Reference Material (ARM, ATCC, Manassas, VA, USA) was diluted in pre-warmed serum-free DMEM and used as diluent for AAV reference standard and

AAV test article in a series of 10-fold dilution. After removal of medium in the 96-well plate, serially diluted AAV was added at 50 μ l/well from Row A to G, Row H was used for the negative control. The set was repeated for Column 2 to 10. Column 11 was used as an uninfected control. After incubation for 2 hours, pre-warmed complete DMEM was added at 50 μ l/well and incubated for two days. The cells were lysed with 10 μ l 10x lysis buffer (1% SDS, 10 mM Tris, 10 mM EDTA, 0.2 mg/ml Proteinase K, pH 8.0) at 37°C for 1 hour, 55 °C for 1 hour and 9°C for 10 minutes. The processed samples were diluted at 1:100 and quantified by TaqMan-qPCR following the procedures used for qPCR titering.

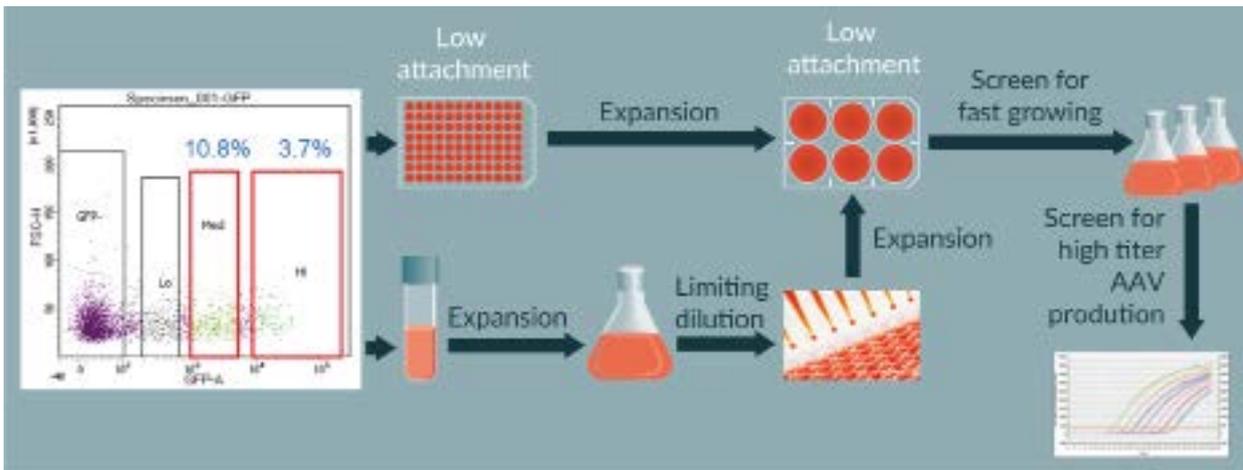
RESULTS

Isolation of clonal suspension HEK293 cells with high AAV productivity

The heterogeneous ATCC suspension HEK293 cells were used to isolate clonal cells for high AAV productivity. As the control Invitrogen clonal suspension HEK293 cells grow in FreeStyle 293 medium, we first adapted the ATCC cells into this growth medium until cell viability was consistently over 90% by Vi-Cell analysis. Next, we hypothesized that AAV productivity by triple transfection may positively correlate with cell transfection efficiency. Therefore, the ATCC cells were transfected with GFP-expressing plasmids and then subjected to cell sorting for GFP-positive transfected cells (Figure 2A). Due to extensive cell death in the GFP-high population, likely attributed to GFP overexpression, we selected

► **FIGURE 2A**

Strategy for identification of single cell clones of suspension HEK293 cell with high AAV productivity.



ATCC suspension HEK293 cells were transfected with GFP-expressing plasmids and GFP-positive (Med and Hi) cells were sorted into single cells in 96-well plates (top pipeline) or collected as pools (bottom pipeline). The pools were plated at single cell level in 96-well plates later by limiting dilution. The survived and expanded cells were screened for AAV productivity by triple transfection and qPCR titer analysis

► **FIGURE 2B**

Strategy for identification of single cell clones of suspension HEK293 cell with high AAV productivity.



Two examples of expansion of single cells (left panels) into cell colonies (right panels) in a 96-well plate.

the viable GFP-medium cells for clonal cell isolation. We sorted these cells into pools for recovery and expansion or directly into single cell each well in 96-well plates. Few single cells survived directly in these 96-well plates. Thus we performed additional limiting dilution experiments to seed single cells in 96-well plates using the survived cell pools.

We identified 54 single cell clones from initial screening on Day 1 post plating. Among these clones, 10 sustained growth and developed into colonies (Figure 2B). As the colonies continued to develop and sufficient cell density was reached, the clones were transferred into larger vessels and eventually into shaker flasks (Figure 2A). As viability improved and a decrease in doubling time was observed, Human Serum Albumin and antibiotics were sequentially removed from the media. A single clone (Clonal ID. 5B8) was selected for further development based on survival and rapid growth characteristics.

Virus productivity of AAV/Anc80 in clone 5B8 was assessed

▶ **TABLE 1**

The screening of commercial media for suspension HEK293 cells based on supported cell density and transfection efficiency. ND, not determined.

Medium type	Vendor	Supported cell density (vc/ml)	Supported transfection	Titer (vg/ml)	
				Control	5B8
293 medium 1	Gibco	3–4 E6	No	ND	ND
293 medium 2	Gibco	3–4 E6	Yes (80–90%)	1.83E+09	ND
293 medium 3	Gibco	6–7 E6	Yes (80–90%)	1.56E+09	1.12E+10
293 medium 4	Gibco	1.5 E7	Yes (80–90%)	1.74E+09	ND
293 medium 5	GE	5–6 E6	Yes (10–30%)	1.39E+08	3.49E+09
293 medium 6	GE	5–6 E6	No	ND	3.97E+07
293 medium 7	GE	6–8 E6	Yes (10–30%)	ND	1.22E+09

and compared to a control commercially available suspension HEK293 using a triple transfection method. The average productivity of AAV/Anc80 in the 5B8 clonal cell line was determined to be 1.2E+10 vg/ml (n = 16) (Data not shown).

Optimization of AAV/Anc80 production in shake flasks

In the process of clonal HEK293 isolation, we started screening commercially available HEK293 cell culture media that support high titer AAV production using control suspension HEK293 cells. The initial

screening of five media (Table 1) identified one medium (medium 3, FreeStyle F17) as the best medium for supporting both high cell density and high transfection efficiency. Medium 4 behaved similarly but is not cost efficient for larger scales. In order to further confirm the preliminary result and assess the growth of the 5B8 clone in additional media, we tested new medium 6 and 7 in addition to medium 3 and 5. Following triple transfection and qPCR titering for AAV/Anc80. GFP, we confirmed that Freestyle F17 remained the best medium for cell growth and AAV production by 5B8 cells (Table 1).

▶ **TABLE 2**

Optimization of triple transfection for AAV production in suspension HEK293 cells.

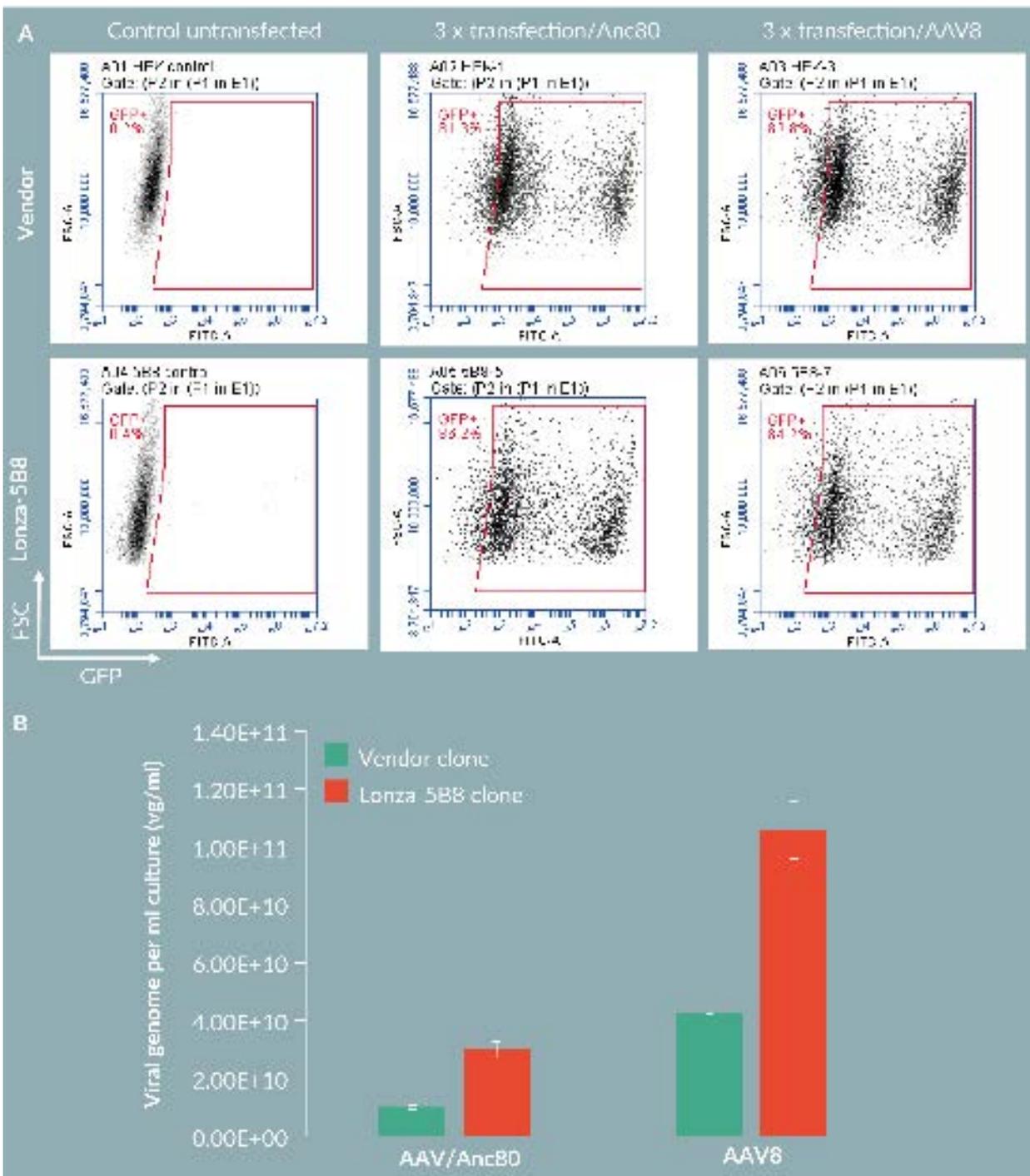
	Lipofectamine		PEIpro		PEI MAX	
	Control	Test	Control	Test	Control	Test
pHelper: pRC: pGOI (molar ratio)	1:1:2	2:1.5:1	1:1:2	2:1.5:1	1:1:2	2:1.5:1
DNA concentration (mg/ml)	1.0	1.5	1.0	1.5	1.0	1.5
Cocktail volume	10%	5%	10%	5%	10%	5%
Reagent: DNA	3:1		2:1		2:1	
Cell density (vc/ml)	1E6		1E6		1E6	

To optimize the transfection process in suspension HEK293 cells, we evaluated the various transfection reagents. As shown in **Table 2**, we compared PEI MAX to PEIpro and

Lipofectamine-LTX (Life Technologies). We observed an approximately 3-fold titer increase using PEI MAX compared to PEIpro. In the same experiment, the DNA amount was

► **FIGURE 3**

Comparison of 5B8 clone to vendor clone for AAV/Anc80 and AAV8 production.



Both 5B8 cells and vendor cells were triple transfected for AAV/Anc80 or AAV8 production. Three days later, the cells were harvested for GFP expression analysis by FACS (A) and for AAV titer analysis by qPCR (B). n = 2.

also varied and different plasmid ratios and different volume of diluent medium were assessed based on data obtained during previous studies [9]. Our data revealed a 2-fold increase in titer in the test condition compared to control.

To determine if a higher cell density can result in increased AAV productivity, we seeded cultures at a different density at transfection. Accordingly, we increased the plasmids concentration proportionally, i.e., 3.2 $\mu\text{g/ml}$ culture for $2\text{E}+06$ vc/ml culture and 4.8 $\mu\text{g/ml}$ for $3\text{E}+06$ vc/ml culture. Interestingly, we successfully detected a proportional increase of AAV titer (Figure 5, 125 ml shake flask). Specifically, the productivity was increased up to $8\text{E}+10$ vg/ml for AAV/Anc80.GFP at $3\text{E}+06$ vc/ml cell density.

To test if the 5B8 clone cells could also support production of other AAV serotypes, we examined AAV8 production. The control HEK293 cells and 5B8 cells were triple transfected with AAV8 or Anc80 Rep/Cap plasmids at $1\text{E}+06$ vc/ml cell density. FACS analysis on the GFP expression in these cells indicated that more than 80% of cells were transfected with each different serotypes in each cell lines, with 5B8 cells showing slightly higher GFP-positive populations (Figure 3A). AAV titer analysis confirmed that the 5B8 clone yielded 2- to 3-fold higher virus titer as compared to control cells. Specifically, we detected about 3-fold titer increase for AAV8 compared to Anc80 (Figure 3B), which is in agreement with the data from Vandenberghe's lab [1]. Therefore, these data indicated that the 5B8 clone supports higher AAV production for other AAV serotypes, such as AAV8, compared

to commercially available control HEK293 cells.

Upstream scale-up to 3 l and 50 l single use bioreactors

To scale up the process from shake flasks to a 50 l scale Stirred Tank Bioreactor (STR), we first tested the production in a 3 l STR. Accordingly, we also tried increased cell density for AAV/Anc80 production in STR (Figure 5). We observed a nearly 2-fold increase of titer when culture was transfected at a cell density higher than $1\text{E}+06$ vc/ml. To evaluate the AAV production process scalability, we performed two 50 l runs, one with pAAV-GFP and another with an undisclosed gene of interest (GOI-2). The complete process is presented in Figure 4. Cell growth between all cell culture vessels were comparable during the cell growth stage. As shown in the Figure 5, both 50 l scale-up runs were comparable to the 3 l STR scale runs in regards to viral titers. However there was at least a 50% decrease from the titers obtained from the shake flask culture. Although further study on the differences will be performed, we were able to produce AAV/Anc80 with two different GOI at $3 \sim 4\text{E}+10$ vg/ml at 50 l scale.

Downstream purification of AAV/Anc80 vectors

Next, we purified and formulated AAV/Anc80.GFP vectors produced from the 50L STR. We accomplished the purification by using a two-column purification system and formulated using

► **FIGURE 4**

Process flow chart for AAV/Anc80 production in 50 l scale.



One vial of 5B8 RCB was thawed and expanded sequentially from shaker flask, WAVE20 to 50 l single-use bioreactor. Cells were triple transfected and allowed for AAV production for three days. Then cells were lysed and treated with Benzonase before clarification by depth filters. Clarified harvest was concentrated and diafiltrated by TFF and subjected to two columns purification. Purified samples were further concentrated and formulated. Finally, drug products were filtered and aseptically filled into glass vials.

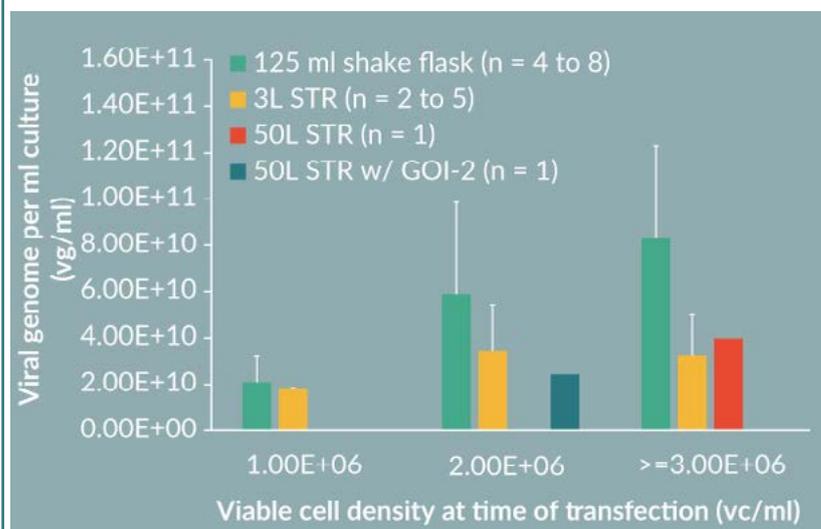
the Hollow Fiber TFF system (Figure 4). We first captured the viral vectors from the column load (concentrated/diafiltrated clarified harvest) using an affinity AVB-Sepharose-HP column (Figure 6A). After elution, we achieved 52% recovery by qPCR analysis (Table 3). We then loaded the sample onto two anion-exchange CIMmultus-QA that served as a polishing step to enrich full capsid vector particles and further remove any remaining impurities (Figure 6B). The yield was approximately 100% following each column run. The purified vectors were then formulated into appropriate formulation buffer using the 100 kD Mi-diKros Hollow Fiber TFF system. The overall recovery was 38% through the purification and formulation processes.

Analytics of purified AAV/Anc80 viral products

To examine the purity of the formulated AAV/Anc80.GFP vectors, we performed silver staining (Figure 7A) and Western blot analysis (Figure 7B). Both analyses suggested that the drug product was highly pure with no detectable capsid degradation or cellular impurities. We also performed negative stain TEM analysis on the sample to examine the morphology and percentages of empty and full viral particles. The majority of viruses were full by TEM analysis (Figure 7C). To have a quantitative result for empty and full ratio, we assessed the sample by analytical ultracentrifugation (AUC). The full vector was about 70% measured by AUC. To assess the

FIGURE 5

AAV/Anc80 productivities during the scale-up using 5B8 cells.



Cells were triple transfected at various cell densities and harvested after three days. qPCR analysis was performed to measure the AAV/Anc80 titer at harvest. pAAV-GFP plasmid was used for the production except one 50L run that used another undisclosed transgene (GOI-2).

infectivity of the formulated AAV, we performed TCID₅₀ assay using HeRC32 cells as described in the Materials and Methods section. The specific infectivity of this material was 281 vg /TCID₅₀ Unit, in the range of AAV2 infectivity produced from HEK293 cells as previously reported [9].

DISCUSSION

Here we report a viable, cost efficient and scalable manufacturing platform for novel Anc80 and other AAV serotypes. The platform is based on upstream production by transient transfection of three plasmids in a highly productive clonal suspension HEK293 cell line in a single use bioreactor and downstream purification using a two-column chromatography process. With this platform, we have achieved

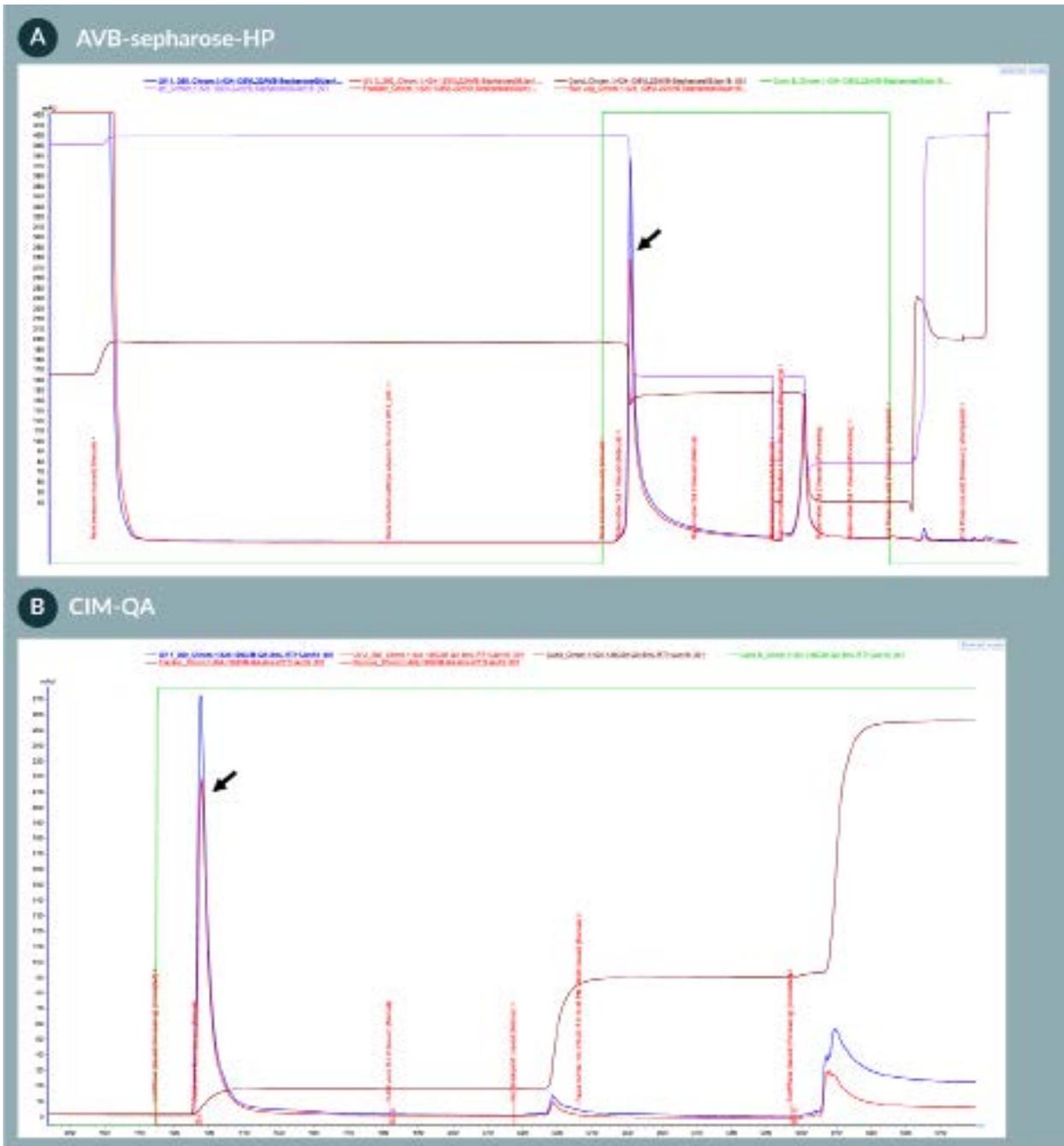
the productivity of approximately 5E+14 purified and formulated Anc80 vector genomes from a 50 l production scale in about 8 weeks.

We isolated a clonal suspension HEK293 cells with superior AAV productivity using a triple

transfection method. Compared to parental ATCC HEK293 cells, an isolated clone, 5B8, increased the AAV titers 5- to 10-fold (data not shown). This may be in part due to better transfection efficiency than the parental pool of cells, as

► **FIGURE 6**

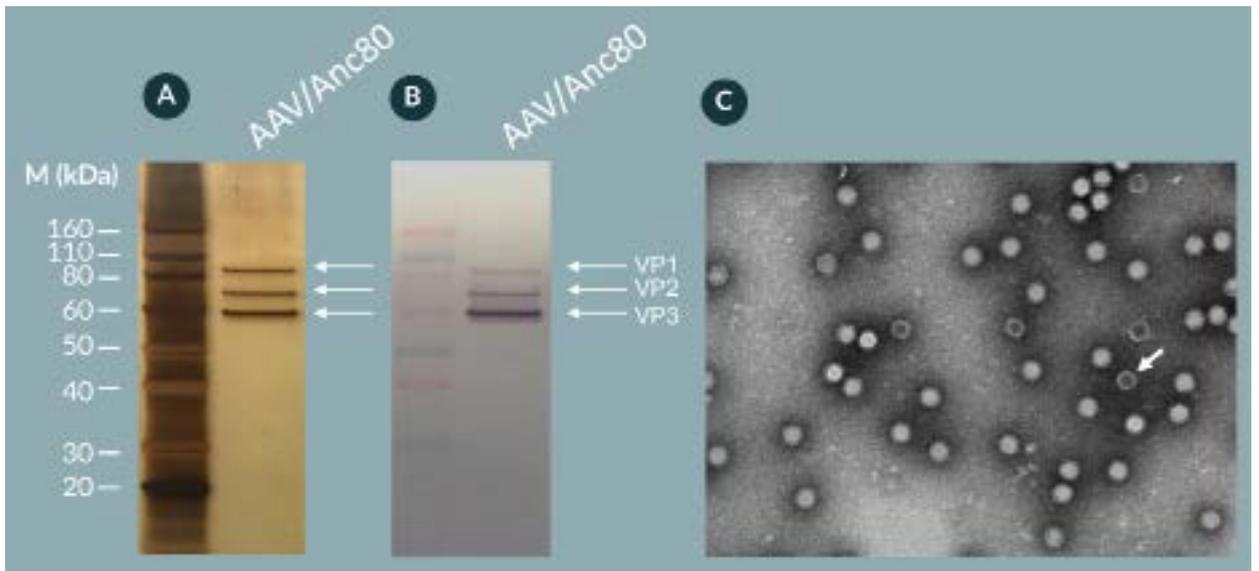
Chromatograms of purification of AAV/Anc80 by two-column chromatography.



TFF diafiltrated samples were first captured by affinity column (A), the eluate from first column was polished by the second ion-exchange column to further purify and enrich full AAV particles (B). Arrows indicate the virus-containing peaks.

► FIGURE 7

Analysis of final AAV/Anc80 drug product.



The formulated AAV/Anc80.GFP sample from 50L production was analyzed by silver staining (A) and Western blot using Capsid-specific antibodies (B). The sample was also subjected to negative staining and transmission electron microscopy analysis for the percentage of full virus (C). The arrow indicates an empty virus with dark center.

the clone was selected based upon sorting for easily transfected cells. When we compared the 5B8 clone with control Invitrogen cells, both showed high and comparable transfection efficiency (over 80%). However, the 5B8 clone performed two to three times better than the control Invitrogen cells in AAV production for both Anc80 and AAV8. The 5B8 cell line was further characterized for stability, identity, bioburden

and mycoplasma testings. A cGMP cell bank of clone 5B8 is in production and will be available through Lonza. Consequently, this high producer HEK293 clone provides an excellent platform for the clinical and commercial production of Anc80 and other serotypes of AAV.

We experienced some productivity loss during the scale up from shake flask to 3L and 50L STRs. This observation suggested the

► TABLE 3

Summary of the analytical results of AAV/Anc80.GFP vector purification and formulation.

Purification/formulation	Sample name	Titer (vg/ml)	Volume (ml)	Total (vg)	Step recovery (%)
AVB	Column load	1.26E+11	3600	4.54E+14	100
	Eluate	1.84E+12	127	2.34E+14	52
CIM-QA (2x runs)	Column load	6.82E+10	1220	8.32E+13	100
	Eluate	2.17E+12	42	9.11E+13	110
Formulation	Pre-formulate	2.85E+12	78	2.22E+14	100
	Formulated	1.18E+13	14.6	1.72E+14	77
	Formulated/filtered DP	1.01E+13	17	1.72E+14	77

transfection mix prepared in WAVE bags for use in STRs was not as efficient as the transfection mix vortexed in tubes for use in shake flasks. Currently, we are working on the improvement of mixing of DNA and PEI for bioreactors.

Our downstream purification process is robust and scalable compared to traditional ultracentrifugation methods. The process involves a first step of affinity chromatography, followed by an anion-exchange polishing step. The virus yield following AVB-Sepharose column purification step was approximately 50%. This recovery rate is acceptable and has been reproducible at various scales. However, additional yield improvement studies will be conducted. In addition, we have tested other commercially available affinity resins but have not achieved reproducible results with different feedstreams over various runs. For the second column, a CIM-QA polishing column was used to further purify and enrich full viruses. Full capsid vector ratio of the final formulated product was initially 45% measured by AUC in the experiment. In the subsequent experiments with further improvements in the process, the percent of full capsid was enriched to higher level (up to 75%) by optimizing the chromatography elution step. Previously, Grieger et al. reported the purification of AAV from HEK293 cell lysate by iodixanol gradient followed by ion exchange chromatography [9], which posed a challenge for scale-up in GMP setting. Therefore, our two-column purification strategy provides a fully scalable and robust solution for AAV GMP purification processes.

While this process is a good near term solution, we are currently developing a transfection-free stable producer cell platform, which is expected to be a more robust, safe and cost-efficient process. The new stable cells would integrate necessary helper genes, Rep/Cap and GOI in the cell genome, allowing for large scale productions of AAV upon an addition of inducing agents, such as small chemicals, and thus eliminating the need of large amount of plasmids and tedious transfection steps. For now, transient transfection in a suspension format is a good bridging solution that provides a simple, fast and scalable process.

FINANCIAL & COMPETING INTERESTS DISCLOSURE

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